

# Preparation of amorphous $\text{Si}_3\text{N}_4$ -C plate by chemical vapour deposition

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Chemical vapour deposition of a Si-N-C system has been studied by using  $\text{SiCl}_4$ ,  $\text{NH}_3$ ,  $\text{H}_2$  and  $\text{C}_3\text{H}_8$  as source gases at deposition temperatures ( $T_{\text{dep}}$ ) of 1100 to 1600°C, and total gas pressures ( $P_{\text{tot}}$ ) of 30 to 100 torr. To control the amount of carbon in these deposits the propane gas flow rate [ $FR(\text{C}_3\text{H}_8)$ ] was varied from 0 to 200  $\text{cm}^3 \text{min}^{-1}$ . Homogeneous plate-like amorphous deposits were successfully prepared at  $T_{\text{dep}} = 1100$  to 1300°C,  $P_{\text{tot}} = 30$  to 70 torr and  $FR(\text{C}_3\text{H}_8) = 25$  to 100  $\text{cm}^3 \text{min}^{-1}$ . The deposits were composed of amorphous silicon nitride and carbon and the carbon content increased up to 10 wt% with increasing  $FR(\text{C}_3\text{H}_8)$ . The surfaces of the deposits had a pebble-like structure.

## 1. Introduction

In view of their good thermal and mechanical properties and oxidation resistance, silicon nitride ( $\text{Si}_3\text{N}_4$ ) and silicon carbide (SiC) are promising materials for high temperature gas turbine applications [1]. Recently, materials composed of Si, N and C have been extensively investigated for possible uses as new high temperature materials. Parr *et al.* [2] and Lange [3] prepared  $\text{Si}_3\text{N}_4$ -SiC composites using SiC powders by reaction-sintering and hot-pressing, respectively, to improve the mechanical properties of  $\text{Si}_3\text{N}_4$  sintered bodies.

Nickl and Braunmühl [4] have studied chemical vapour deposition (CVD) of the Si-N-C system by using  $\text{SiCl}_4$ ,  $\text{CCl}_4$ ,  $\text{H}_2$  and  $\text{N}_2$  as source gases and obtained Si + SiC +  $\text{Si}_3\text{N}_4$  deposits. However, they have not provided any information on the properties of these deposits. Jacobson [5] has obtained an amorphous  $\text{Si}_3\text{N}_4$  powder containing 0.1 to 5 wt% of carbon by CVD using  $\text{SiCl}_4$ ,  $\text{NH}_3$ ,  $\text{N}_2$  and  $\text{CH}_4$ . He has reported that this powder is useful in the preparation of fully dense SiAlON ceramics.

In a CVD study of the Si-N system, we succeeded in preparing massive amorphous and crystalline CVD- $\text{Si}_3\text{N}_4$  at high deposition speeds (maximum 1.2  $\text{mm h}^{-1}$ ) using  $\text{SiCl}_4$ ,  $\text{NH}_3$  and  $\text{H}_2$

[6, 7], and investigated the properties of the CVD- $\text{Si}_3\text{N}_4$  [8-11]. Using the same apparatus and methods for preparing CVD- $\text{Si}_3\text{N}_4$ , the CVD of a Si-N-C system was carried out by adding  $\text{C}_3\text{H}_8$  gas to the source gases. This paper describes the effects of CVD variables (deposition temperature, total gas pressure and gas flow rate) on the deposition of the Si-N-C system.

## 2. Experimental procedure

### 2.1. Sample preparation

The experimental set-up is illustrated in Fig. 1. The graphite substrate (40 mm × 12 mm × 2 mm) was heated by transmitting an electric current. The deposition temperature,  $T_{\text{dep}}$ , was measured using a two-colour pyrometer. The total gas pressure,  $P_{\text{tot}}$ , was regulated in the range of 30 to 100 torr\* by needle valves.  $\text{SiCl}_4$  vapour (purity: 99.9%),  $\text{NH}_3$  gas (99.9%),  $\text{H}_2$  gas (99.9999%) and  $\text{C}_3\text{H}_8$  gas (94.5%) were used as source gases. The  $\text{SiCl}_4$  container was maintained at 20°C and the saturated vapour of  $\text{SiCl}_4$  was carried with  $\text{H}_2$  gas. The  $\text{SiCl}_4$  vapour and  $\text{NH}_3$  gas were separately introduced through a double tube nozzle into the CVD chamber to prevent premature vapour reaction [6]. In this present investigation,  $\text{NH}_3$  gas and ( $\text{SiCl}_4 + \text{C}_3\text{H}_8 + \text{H}_2$ ) gases were introduced through the

\*1 atm = 760 torr = 0.1013 MPa.

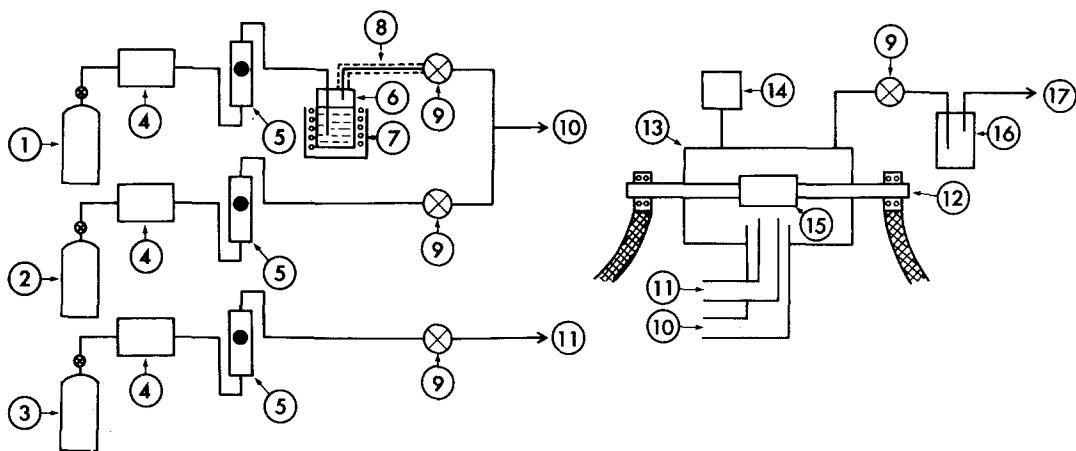


Figure 1 Schematic diagram of deposition apparatus. (1)  $H_2$  gas; (2)  $C_3H_8$  gas; (3)  $NH_3$  gas; (4) gas purifier; (5) flow meter; (6)  $SiCl_4$  reservoir; (7) constant temperature bath; (8) ribbon heater; (9) pressure regulator; (10)  $SiCl_4 + H_2 + C_3H_8$  gas inlet; (11)  $NH_3$  gas inlet; (12) copper electrode; (13) reaction chamber; (14) manometer; (15) graphite heater (substrate); (16) cold trap; (17) rotary pump.

inner and outer tubes, respectively. The gas flow rate was measured by a flow meter. In reference to previous work [6, 12, 13], the flow rates of  $H_2$  and  $NH_3$  gases [ $FR(H_2)$  and  $FR(NH_3)$ ] were respectively fixed at 700 and  $60\text{ cm}^3\text{ min}^{-1}$ . The flow rate of propane gas [ $FR(C_3H_8)$ ] was controlled in the range of 0 to  $200\text{ cm}^3\text{ min}^{-1}$ . The deposition conditions are summarized in Table I.

## 2.2. Microstructure and chemical composition

The as-deposited surfaces and the fracture surfaces were coated with gold (5 to 10 nm in thickness) and observed by means of scanning electron microscopy (SEM) (Hitachi-Akashi: MSM-4). The polished surfaces of the deposits were examined by electron spectroscopy for chemical analysis (ESCA) (AEI-Kokusai Denki: AEI-ES200). The structures of various parts of plate-like deposits were examined by an X-ray diffractometer (Ni filtered  $K_\alpha$ , JEOL: DX-GO-S). The content of carbon was determined by chemical analysis, and the contents

TABLE I

Deposition conditions	
Deposition temperature, $T_{\text{dep}}$ ( $^\circ\text{C}$ )	1100 to 1600
Total gas pressure, $P_{\text{tot}}$ (torr)	30 to 100
Gas flow rate, $FR(\text{cm}^3\text{ min}^{-1})$	
$FR(H_2)$	700
$FR(SiCl_4)$	170
$FR(NH_3)$	60
$FR(C_3H_8)$	0 to 200
Deposition time, $t$ (h)	0.5 to 8

of Si and N were examined by electron probe microanalysis (EPMA) (Shimadzu: EMX-SM) using amorphous CVD- $Si_3N_4$  as a standard sample.

## 3. Results

### 3.1. Preparation of Si-N-C deposits

Figs 2 to 5 show the characteristics of Si-N-C deposits obtained under various CVD conditions.

At  $T_{\text{dep}} = 1100$  and  $1200^\circ\text{C}$ , as indicated by X in Fig. 2, the deposition temperature became uncontrollable above  $P_{\text{tot}} = 80$  torr due to the formation of by-product powders in the vapour phase. Homogeneous plate-like amorphous deposits were also obtained at  $P_{\text{tot}} = 30$  to 70 torr and

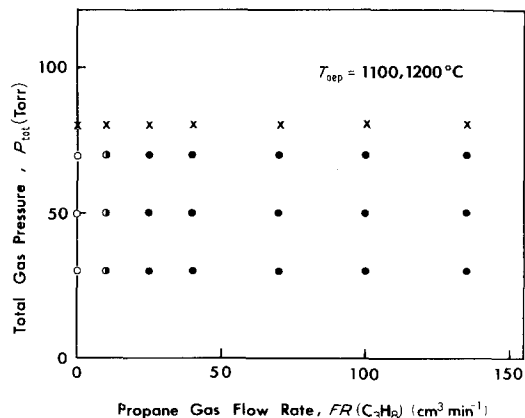


Figure 2 Effect of the propane gas flow rate [ $FR(C_3H_8)$ ] and the total gas pressure ( $P_{\text{tot}}$ ) on the deposits prepared at  $T_{\text{dep}} = 1100$  and  $1200^\circ\text{C}$ .  $\circ$ : amorphous  $Si_3N_4$ ,  $\bullet$ : amorphous  $Si_3N_4 +$  amorphous deposit,  $\bullet$ : homogeneous amorphous deposit, X: uncontrollable conditions.

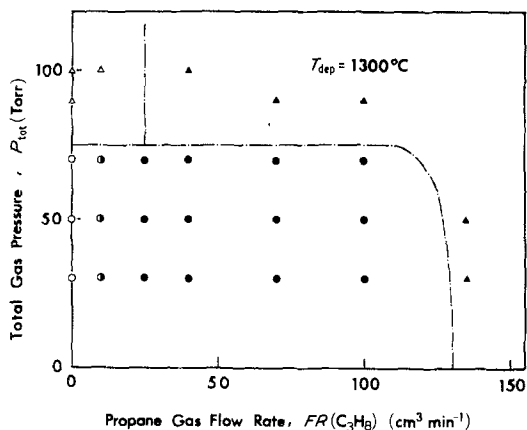


Figure 3 Effect of the propane gas flow rate [ $FR(C_3H_8)$ ] and the total gas pressure ( $P_{tot}$ ) on the deposits prepared at  $T_{dep} = 1300^\circ C$ . ○: amorphous  $Si_3N_4$ , ◻: amorphous  $Si_3N_4$  + amorphous deposit, ●: homogeneous amorphous deposit, △: amorphous deposit +  $\alpha$ - $Si_3N_4$ , ▲: amorphous deposit + pyrolytic carbon.

$FR(C_3H_8) = 25$  to  $135\text{ cm}^3\text{ min}^{-1}$ . The colours of these deposits were, respectively, white, white plus black, and black at  $FR(C_3H_8) = 0, 10$  and  $25\text{ cm}^3\text{ min}^{-1}$  or above, respectively.

At  $T_{dep} = 1300^\circ C$ , as shown in Fig. 3, homogeneous amorphous deposits were obtained at  $P_{tot} = 30$  to  $70$  torr and in the range of  $FR(C_3H_8) = 25$  to  $100\text{ cm}^3\text{ min}^{-1}$ , and the colours of the deposits were similar to those prepared at  $T_{dep} = 1100$  and  $1200^\circ C$ . Pyrolytic carbon or  $\alpha$ - $Si_3N_4$  was co-deposited heterogeneously with the amorphous deposits in the regions indicated by ▲ and △ in Fig. 3.

At  $T_{dep} = 1400^\circ C$ , as shown in Fig. 4, the

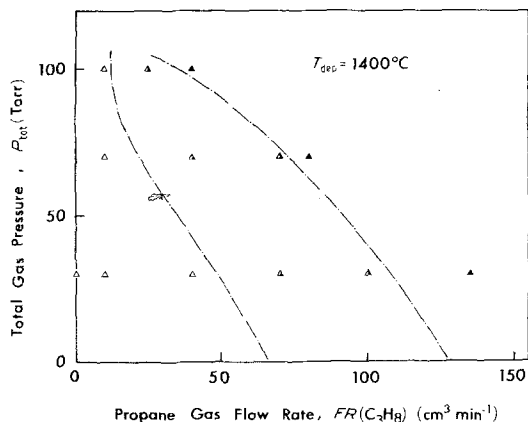


Figure 4 Effect of the propane gas flow rate [ $FR(C_3H_8)$ ] and the total gas pressure ( $P_{tot}$ ) on the deposits prepared at  $T_{dep} = 1400^\circ C$ . △: amorphous deposit +  $\alpha$ - $Si_3N_4$ , ▲: amorphous deposit +  $\alpha$ - $Si_3N_4$  + pyrolytic carbon, ▲: amorphous deposit + pyrolytic carbon.

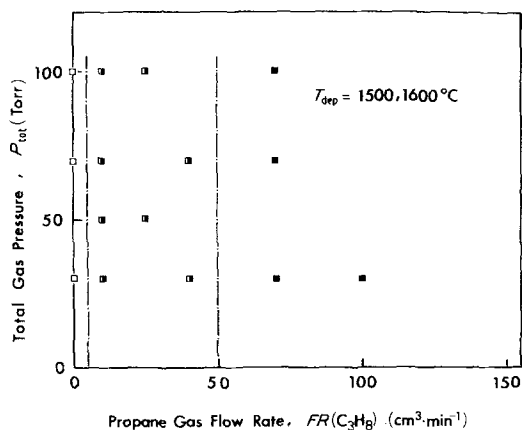


Figure 5 Effect of the propane gas flow rate [ $FR(C_3H_8)$ ] and the total gas pressure ( $P_{tot}$ ) on the deposits prepared at  $T_{dep} = 1500$  and  $1600^\circ C$ . ◻:  $\alpha$ - $Si_3N_4$ , ■:  $\alpha$ - $Si_3N_4$  +  $\beta$ - $SiC$ , ■:  $\beta$ - $SiC$  + pyrolytic carbon.

characteristics of the deposits formed were also dependent on  $P_{tot}$  and  $FR(C_3H_8)$ . For example, at  $P_{tot} = 30$  torr, amorphous deposits and  $\alpha$ - $Si_3N_4$  were heterogeneously co-deposited at  $FR(C_3H_8) = 0$  to  $40\text{ cm}^3\text{ min}^{-1}$ , whereas amorphous deposits and pyrolytic carbon were heterogeneously co-deposited at  $FR(C_3H_8) = 135\text{ cm}^3\text{ min}^{-1}$ .

At  $T_{dep} = 1500$  and  $1600^\circ C$ , as shown in Fig. 5,  $\alpha$ - $Si_3N_4$  was always obtained at  $FR(C_3H_8) = 0\text{ cm}^3\text{ min}^{-1}$  regardless of  $P_{tot}$ . A heterogeneous mixture of  $\alpha$ - $Si_3N_4$  and  $\beta$ - $SiC$  was obtained at  $FR(C_3H_8) = 10$  to  $40\text{ cm}^3\text{ min}^{-1}$ , and  $\beta$ - $SiC$  and pyrolytic carbon were heterogeneously co-deposited above  $FR(C_3H_8) = 70\text{ cm}^3\text{ min}^{-1}$ .

### 3.2. Morphology of deposits

A typical homogeneous amorphous deposit obtained in the present work is shown in Fig. 6b and compared with the amorphous CVD- $Si_3N_4$  (Fig. 6a). The colours of these deposits were respectively white and black. Fig. 7 shows the morphology of the deposits in Fig. 6, which were observed by SEM. Both surfaces indicated a pebble-like structure with a diameter of  $0.1$  to  $0.3\text{ mm}$ . There appears to be no difference between the homogeneous amorphous deposit obtained in the present experiments and the amorphous CVD- $Si_3N_4$ .

The density and deposition rate of the homogeneous amorphous deposits obtained here were respectively  $2.80$  to  $3.00\text{ g cm}^{-3}$  and  $0.07$  to  $0.6\text{ mm h}^{-1}$  depending on deposition conditions. Detailed results on the density and deposition rate will be reported in a forthcoming paper.

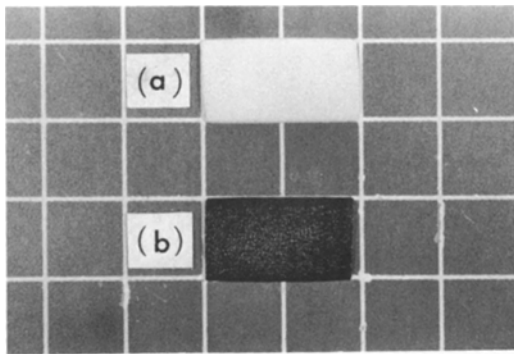


Figure 6 Surfaces of the amorphous  $\text{Si}_3\text{N}_4$  and the homogeneous amorphous deposit prepared at  $T_{\text{dep}} = 1300^\circ\text{C}$ ,  $P_{\text{tot}} = 30$  torr and (a)  $FR(\text{C}_3\text{H}_8) = 0 \text{ cm}^3 \text{ min}^{-1}$  and (b)  $FR(\text{C}_3\text{H}_8) = 100 \text{ cm}^3 \text{ min}^{-1}$ . (1 division = 12.5 mm).

### 3.3. Carbon analysis

Fig. 8 indicates the distribution of Si, N and C in a cross-section of the homogeneous amorphous deposit prepared at  $T_{\text{dep}} = 1300^\circ\text{C}$ ,  $P_{\text{tot}} = 30$  torr and  $FR(\text{C}_3\text{H}_8) = 70 \text{ cm}^3 \text{ min}^{-1}$ . EPMA revealed that Si, N and C were uniformly distributed in the deposit. Similar results were observed in all the deposits marked by  $\bullet$  in Figs 2 and 3. The Si to N atomic ratio determined by the EPMA was about 3/4. Thus, the homogeneous amorphous deposits containing carbon are abbreviated as Am.CVD-( $\text{Si}_3\text{N}_4$ -C).

Fig. 9 shows the effect of  $FR(\text{C}_3\text{H}_8)$  on carbon content for Am.CVD-( $\text{Si}_3\text{N}_4$ -C) prepared at  $T_{\text{dep}} = 1100$  to  $1300^\circ\text{C}$ . The carbon content increased with increasing  $FR(\text{C}_3\text{H}_8)$ , and it was minimally affected by  $T_{\text{dep}}$  and  $P_{\text{tot}}$  as shown in Figs 10 and 11.

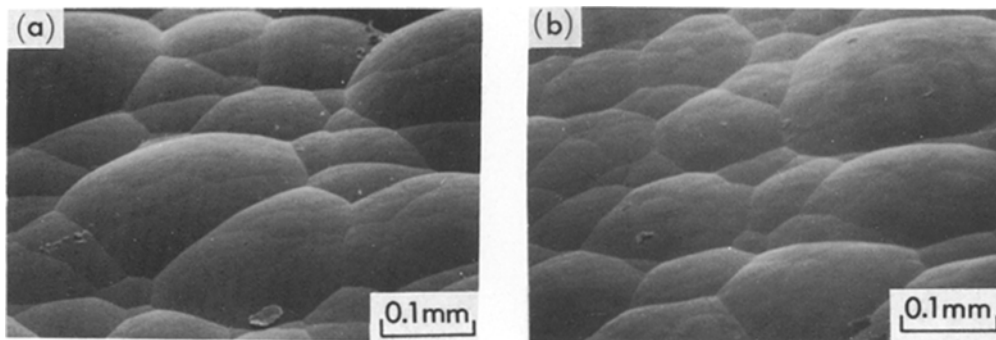


Figure 7 Scanning electron micrographs of the surfaces of the amorphous  $\text{Si}_3\text{N}_4$  and the homogeneous amorphous deposit prepared at  $T_{\text{dep}} = 1300^\circ\text{C}$ ,  $P_{\text{tot}} = 30$  torr and (a)  $FR(\text{C}_3\text{H}_8) = 0 \text{ cm}^3 \text{ min}^{-1}$  and (b)  $FR(\text{C}_3\text{H}_8) = 100 \text{ cm}^3 \text{ min}^{-1}$ .

### 3.4. Structure of carbon

Values of the lattice constant ( $c_0$ ) of pyrolytic carbon in the heterogeneous deposits prepared at  $T_{\text{dep}} = 1500$  and  $1600^\circ\text{C}$  were 0.689 and 0.690 nm. The carbon in Am.CVD-( $\text{Si}_3\text{N}_4$ -C) showed no X-ray reflection, though an ESCA indicated a signal of a free carbon.

## 4. Discussion

### 4.1. Compounds of the Si-N-C system

Schutzenberger and Colson [14] and Weiss and Engelhardt [15] tried to prepare compounds of a Si-N-C system by heating a mixture of silica and carbon in a nitrogen stream, and detected  $\text{Si}_2\text{C}_2\text{N}$  and  $\text{Si}_3\text{C}_3\text{N}$ , respectively. At present, however, evidence shows that there are no compounds of the Si-N-C system [16, 17].

The deposits obtained in the present work were composed of amorphous  $\text{Si}_3\text{N}_4$ , carbon,  $\alpha$ - $\text{Si}_3\text{N}_4$  and  $\beta$ -SiC as shown in Figs 2 to 5.

Rassaerts and Schmidt [18] proposed a phase diagram of a Si-N-C system at  $P_{\text{tot}} = 760$  torr by using thermodynamic data on  $\text{Si}_3\text{N}_4$ , SiC and  $\text{C}_2\text{N}_2$ , as represented in Fig. 12. Lilov *et al.* [19] calculated the thermodynamic data for the Si-N-C system, and showed that  $\text{Si}_3\text{N}_4$  could not exist at  $P_{\text{tot}} = 4$  torr and above  $1478^\circ\text{C}$ . The decomposition temperature of  $\text{Si}_3\text{N}_4$  in the presence of carbon has been variously reported as mentioned above.

The present experimental conditions are indicated by the broken line in Fig. 12. The  $\text{N}_2$  partial pressure in the reaction chamber might be considerably lowered by the consumption of  $\text{NH}_3$  by the formation of large amounts of  $\text{Si}(\text{NH})_2$  and  $\text{NH}_4\text{Cl}$  powders [20]. Moreover, it was apparent

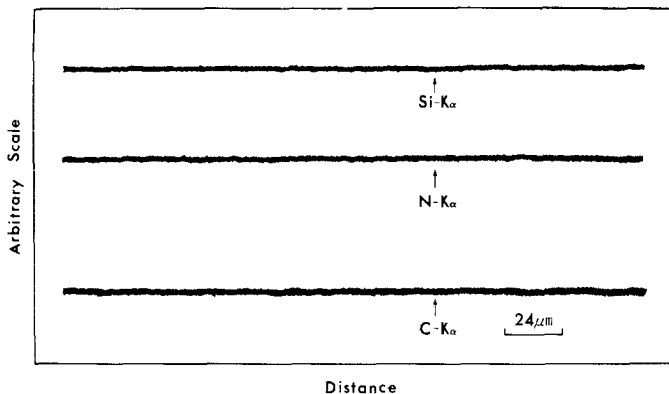


Figure 8 The results of an EPMA for Si, N and C content of cross-sectional surface of the homogeneous amorphous deposit prepared at  $T_{\text{dep}} = 1300^\circ\text{C}$ ,  $P_{\text{tot}} = 30$  torr and  $FR(\text{C}_3\text{H}_8) = 70$   $\text{cm}^3$   $\text{min}^{-1}$ .

that SiC was not formed below  $1400^\circ\text{C}$ . Thus, the present deposition conditions seem to be in the hatched area in Fig. 12.

#### 4.2. CVD of a Si–N–C system

Nickl and Braumühl [4] studied CVD of a Si–N–C system using  $\text{SiCl}_4 + \text{N}_2 + \text{H}_2 + \text{CCl}_4$

gases at  $T_{\text{dep}} = 1100$  to  $1300^\circ\text{C}$  and  $P_{\text{tot}} = 715 \pm 15$  torr, and obtained a three-phase deposition mixture of Si, SiC and  $\text{Si}_3\text{N}_4$ . The structure of  $\text{Si}_3\text{N}_4$  in the deposits was amorphous below  $T_{\text{dep}} = 1200^\circ\text{C}$ . At  $T_{\text{dep}} = 1300^\circ\text{C}$ ,  $\alpha\text{-Si}_3\text{N}_4$  was also deposited.

In the present experiments, as shown in Figs 2 and 3, Am.CVD-( $\text{Si}_3\text{N}_4$ -C) was formed without the formation of SiC at  $T_{\text{dep}} = 1100$  to  $1300^\circ\text{C}$  and  $P_{\text{tot}} = 30$  to 70 torr. Moreover, as shown in Fig. 5, Am.CVD-( $\text{Si}_3\text{N}_4$ -C) was not obtained at  $T_{\text{dep}} = 1500$  and  $1600^\circ\text{C}$ . In the present work, carbon was supposed to exist as a free carbon in Am.CVD-( $\text{Si}_3\text{N}_4$ -C), although carbon exists as a combined carbon (SiC) in the results of Nickl and Braumühl. This difference seems to be caused by the variation in the CVD conditions.

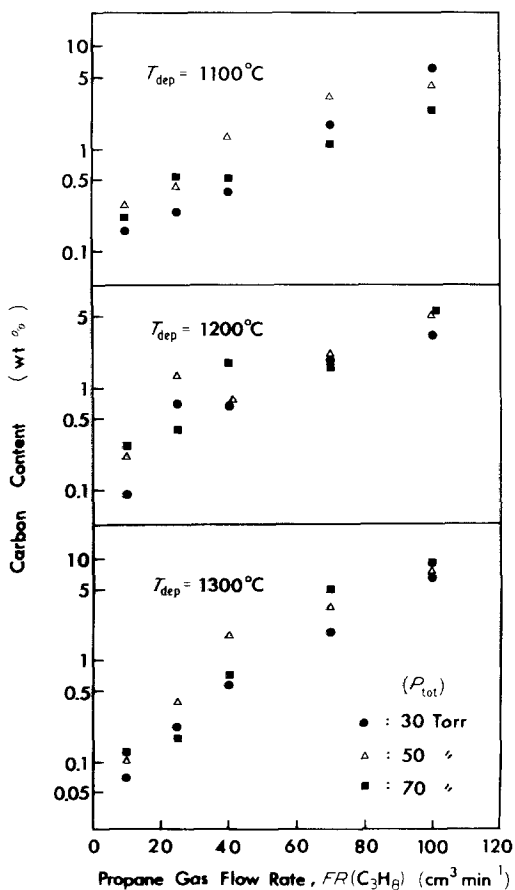


Figure 9 Effect of the propane gas flow rate [ $FR(\text{C}_3\text{H}_8)$ ] on the carbon content of the homogeneous amorphous deposits prepared at  $T_{\text{dep}} = 1100$  to  $1300^\circ\text{C}$ .

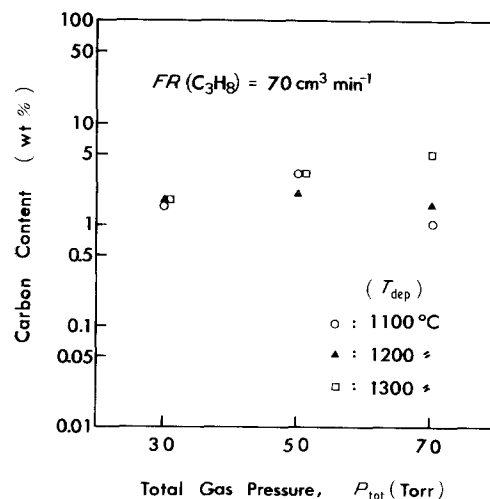


Figure 10 Effect of the total gass pressure ( $P_{\text{tot}}$ ) on the carbon content of the homogeneous amorphous deposits prepared at  $FR(\text{C}_3\text{H}_8) = 70$   $\text{cm}^3$   $\text{min}^{-1}$ .

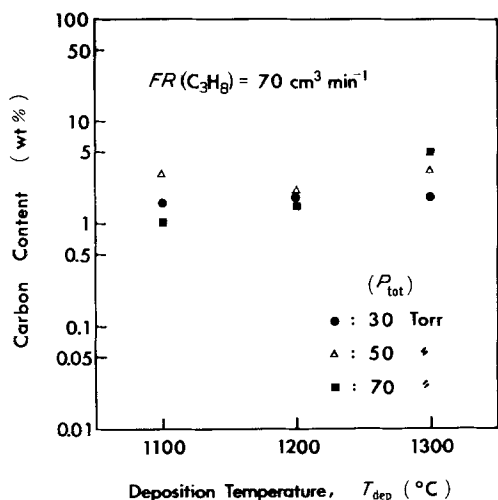


Figure 11 Effect of the deposition temperature ( $T_{dep}$ ) on the carbon content of the homogeneous amorphous deposits prepared at  $FR(C_3H_8) = 70 \text{ cm}^3 \text{ min}^{-1}$ .

### 4.3. Crack formation in the deposits

Airey *et al.* [21] reported that the amount of cracks formed in the amorphous CVD- $\text{Si}_3\text{N}_4$  decreases with increasing  $T_{dep}$  and with decreasing deposition rate. They thought that the higher  $T_{dep}$  and the lower deposition rate, the more readily the stress relief occurs accompanied by the cluster rearrangement. In the present experiments many visible cracks were found in Am.CVD- $(\text{Si}_3\text{N}_4\text{-C})$  prepared at high  $P_{tot}$  and low  $T_{dep}$ . This is in good rearrangement. In the present experiments, many Kohler [22] reported that impurity particles cause crack formation in the amorphous CVD- $\text{Si}_3\text{N}_4$ .

The present experiments showed that crack formation was also remarkable in a high carbon Am.CVD- $(\text{Si}_3\text{N}_4\text{-C})$ . It appears that carbon is present as a second phase in Am.CVD- $(\text{Si}_3\text{N}_4\text{-C})$ .

On the other hand, as shown in Fig. 5,  $\alpha\text{-Si}_3\text{N}_4$  and  $\beta\text{-SiC}$  were heterogeneously co-deposited under the conditions of  $T_{dep} = 1500, 1600^\circ \text{C}$  and  $FR(C_3H_8) = 25 \text{ to } 40 \text{ cm}^3 \text{ min}^{-1}$ . In these cases, cracks generated at the phase boundary of  $\alpha\text{-Si}_3\text{N}_4$  and  $\beta\text{-SiC}$  and extended to the  $\alpha\text{-Si}_3\text{N}_4$  phase. This crack formation was thought to be caused by the difference in the thermal expansion coefficients of  $\text{Si}_3\text{N}_4$  and  $\text{SiC}$ . Almost no cracks were observed in the deposits composed of  $\beta\text{-SiC}$  and pyrolytic carbon.

### 4.4. Structure of carbon

As described in Section 3.4., the values of lattice constant,  $c_0$ , of the pyrolytic carbon were 0.689 and 0.690 nm. These values are in good agreement with the previously published data on pyrolytic carbon [23]. The structure of carbon in Am.CVD- $(\text{Si}_3\text{N}_4\text{-C})$  is not clear and further investigations using positron annihilation and neutron diffraction are presently being conducted.

## 5. Conclusions

(1) Homogeneous amorphous deposits [Am.CVD- $(\text{Si}_3\text{N}_4\text{-C})$ ] were obtained at deposition temperatures ( $T_{dep}$ ) of 1100 to 1300°C, total gas pressures ( $P_{tot}$ ) of 30 to 70 torr and propane gas flow rates [ $FR(C_3H_8)$ ] of 25 to 100  $\text{cm}^3 \text{ min}^{-1}$ .

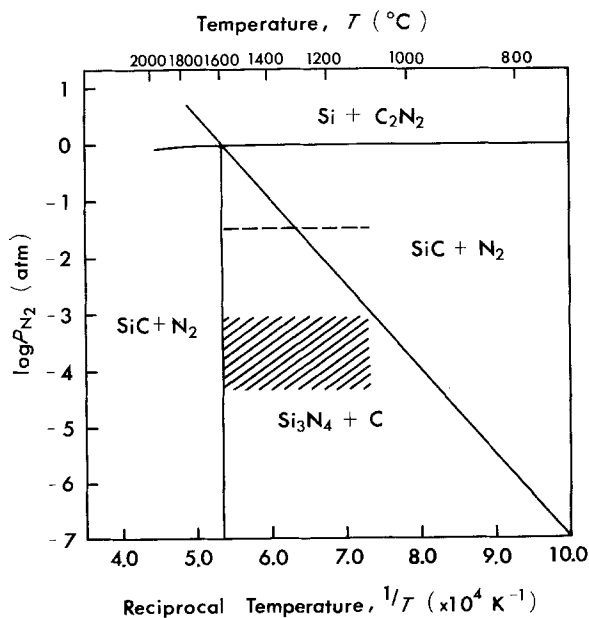


Figure 12  $\log P_{N_2} - 1/T$  diagram of the Si-N-C system [18].

(2) Am.CVD-(Si<sub>3</sub>N<sub>4</sub>-C) was not obtained above  $P_{\text{tot}} = 100$  torr and above  $FR(C_3H_8) = 135 \text{ cm}^3 \text{ min}^{-1}$  at  $T_{\text{dep}} = 1300^\circ \text{C}$ . Above  $T_{\text{dep}} = 1400^\circ \text{C}$ , in all deposition conditions Am.CVD-(Si<sub>3</sub>N<sub>4</sub>-C) was not obtained.

(3) The surface of Am.CVD-(Si<sub>3</sub>N<sub>4</sub>-C) was black and showed a pebble-like structure.

(4) The carbon content in Am.CVD-(Si<sub>3</sub>N<sub>4</sub>-C) increased up to 10 wt % with increasing  $FR(C_3H_8)$ .

(5) The carbon in Am.CVD-(Si<sub>3</sub>N<sub>4</sub>-C) showed no X-ray diffraction peaks, but a signal indicating a free carbon was detected by ESCA.

(6) The Si to N ratio in Am.CVD-(Si<sub>3</sub>N<sub>4</sub>-C) was about 3/4.

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